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## CLAIMS

1. A process for preparation of a monoketal compound of the structure



said process comprising reacting 1,4-cyclohexanedione of the structure

with a diol of the structure

in a halogenated organic solvent in the presence of an acid catalyst, wherein X is a substituted or unsubstituted ethylene or propylene.

- 2. The process of claim 1, wherein said diol is selected from the group consisting of ethylene glycol, propylene glycol, neopentyl glycol or 1,3-propanediol.
- 3. The process of claim 1, wherein said diol is neopentyl glycol of the structure

- 4. The process of claim 3, further comprising
  - a. converting said monoketal compound to an alkylamino ketal of

- b. reacting said alkylamino ketal with 4-carboxamidophenylhydrazine.
- 5. The process of claim 1, wherein said halogenated organic solvent is a C<sub>1</sub>-C<sub>3</sub> haloalkane.
- 6. The process of claim 5, wherein said C<sub>1</sub>-C<sub>3</sub> haloalkane is selected from the group consisting of chloroform, dichloromethane, dichloroethane, carbon tetrachloride and mixtures thereof.
- 7. The process of claim 5, wherein said  $C_1$ - $C_3$  haloalkane is dichloromethane.
- 8. The process of claim 5, wherein said  $C_1$ - $C_3$  haloalkane is chloroform.
- 9. The process of claim 1, wherein the molar ratio of 1,4-cyclohexanedione to 2,2-dimethyl-1,3-propanediol ranges from about 1:1 to about 1:4.
- 10. The process of claim 1, wherein the molar ratio of 1,4-cyclohexanedione to 2,2-dimethyl-1,3-propanediol ranges from about 1:1 to about 1:2.
- 11. The process of claim 1, wherein the molar ratio of 1,4-cyclohexanedione to 2,2-dimethyl-1,3-propane diol is about 1:1.
- 12. The process of claim 1, wherein the weight/volume ratio of 1,4-cyclohexanedione to said halogenated organic solvent ranges from about 1:1 to about 1:20.
- 13. The process of claim 1, wherein the weight/volume ratio of 1,4-cyclohexanedione to said halogenated organic solvent is about 1:8.

- 14. The process of claim 1, wherein the reacting step includes dissolving 1,4-cyclohexanedione and said diol in said halogenated organic solvent and adding said acid catalyst to initiate the reaction.
- 15. The process of claim 1, wherein said acid catalyst is selected from the group consisting of hydrochloric acid, p-toluenesulfonic acid, sulfuric acid, fumaric acid, phthalic acid, oxalic acid and mixtures thereof.
- 16. The process of claim 1, wherein said acid catalyst is sulfuric acid.
- 17. The process of claim 1, wherein said reaction is performed at a temperature of from about 25 to about 50°C.
- 18. The process of claim 1, wherein said reaction is performed at a temperature of from about 25 to about 30°C.
- 19. The process of claim 1, further comprising removing said halogenated solvent to provide a crude residue; contacting said crude residue with an aliphatic or alicyclic hydrocarbon solvent; and removing solid impurities from the mixture.
- 20. The process of claim 19, wherein said aliphatic or alicyclic hydrocarbon solvent is selected from the group consisting of petroleum ether, hexane, n-hexane, cyclohexane, n-heptane, cycloheptane and mixtures thereof.
- 21. The process of claim 19, wherein said aliphatic or alicyclic hydrocarbon solvent is n-heptane.
- 22. The process of claim 19, wherein the removal of by-product(s) is achieved by filtration.
- 23. The process of claim 22, further comprising cooling the mixture of the crude residue and the aliphatic or alicyclic hydrocarbon solvent to a temperature of from about 0 to about 25°C before said filtration.
- 24. The process of claim 23, wherein said reaction mass is cooled to a temperature of about 0-5°C.

- 25. A process for the preparation of 1,4-cyclohexanedione mono-2,2-dimethyl trimethylene ketal, said process comprising:
- a. reacting 1,4-cyclohexanedione and neopentyl glycol in dichloromethane or chloroform in the presence of sulfuric acid at about 25-50°C;
- b. removing dichloromethane or chloroform to provide a crude residue;
- c. combining an aliphatic or alicyclic hydrocarbon solvent with said crude residue to form a mixture;
  - d. cooling said mixture to a temperature of about 0-5°C; and
  - e. filtering the cooled mixture to remove undissolved impurities.